Flowfield Characterization in a LOX/GH<sub>2</sub> Propellant Rocket S. Pal, M. D. Moser, H. M. Ryan, M. J. Foust and R. J. Santoro

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### Statement of Problem

There is a critical shortage of data pertaining to the flowfield characteristics in a liquid propellant rocket chamber for hot-fire conditions. For a liquid oxygen (LOX)/gaseous hydrogen (GH<sub>2</sub>) propellant combination, either shear or swirl coaxial injectors are typically used to atomize the liquid propellant into drops. Understanding the atomization process under hot-fire conditions represents the first step in understanding the subsequent processes of vaporization, mixing and combustion. The flowfield here is two-phase and therefore experiments that detail the intact liquid jet, drop size and velocity, and combustion length are necessary for understanding the physics of the problem.

### Objective of Work

The objective of the current work is to experimentally characterize the flowfield associated with an uni-element shear coaxial injector burning LOX/GH<sub>2</sub> propellants. These experiments were carried out in an optically-accessible rocket chamber operating at a high pressure ( $\approx 400$  psia). Quantitative measurements of drop size and velocity were obtained along with qualitative measurements of the disintegrating jet.

### **Approach**

The experiments were conducted at the Cryogenic Combustion Laboratory at Penn State University. This laboratory provides the capability for firing both gaseous and liquid propellant sub-scale rocket engines. A modular rocket chamber which provides extensive optical access was designed for the experiments. The cross-section of the rocket is 50.8 mm (2 in.) square and the chamber length which can be easily varied was 248 mm (9.75 in.). The flowfield downstream of a shear coaxial injector was characterized using laser-based diagnostic techniques. The inner diameter of the LOX post was 3.43 mm (0.135 in.) and the post was recessed 3.78 mm (0.15 in.). The inner diameter of the fuel annulus was 4.19 mm (0.165 in.) and the outer diameter was 7.11 mm (0.28 in.). The nominal LOX and  $GH_2$  flowrates were 0.11 kg/s (0.25 lbm/s) and 0.021 kg/s (0.047 lbm/s) respectively, thus resulting in a nominal O/F ratio of 5.3:1. These flow rates, coupled with the nozzle dimensions yielded a chamber pressure of 2.74 MPa ( $\approx$  400 psia). The duration of a test run was four seconds.

A Phase Doppler Particle Analyzer (PDPA) was used to measure LOX drop size and velocity at various radial locations for an axial position 63.5 mm (2.5 in.) downstream of the injector face. The measured Sauter Mean diameter (SMD) ranged from 110  $\mu$ m at the centerline to about 60  $\mu$ m at a 9.5 mm (0.375 in.) radial location. At greater radial locations, no drops were observed. The results indicate that under hot-fire conditions, the drops formed from the shear coaxial injector are confined to a narrow circumferential region.

### Conclusions

These experiments represent the first time that drop sizes have been measured under combusting conditions for cryogenic propellants. These results are, in general, encouraging with respect to applications of laser-based diagnostics to LOX/GH<sub>2</sub> uni-element rocket studies. A comprehensive mapping of the flowfield will need to be completed to gain a thorough understanding of the physics of this complex problem.

### Flowfield Characterization in a Liquid Oxygen/Gaseous Hydrogen Propellant Rocket

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### PRESENTATION OUTLINE

Motivation
Background
Objective
Experimental
- Facility
- Rocket chamber
- Diagnostics
Results
Summary

### **MOTIVATION**

### To obtain fundamental data under well characterized conditions

- For gaseous propellant rockets
- For liquid propellant rockets
- For various injector types

### Fundamental data would form the basis for

- Empirical correlation validation
- CFD code validation

### **BACKGROUND**

### Atomization models typically are:

- Anchored to cold flow experimental results

We and Re of cold flow experiments differ by an order of magnitude from actual rocket conditions

Results have to be extrapolated

- Predicted from analytical models based on linear stability theory

### Drop size data for hot-fire conditions would:

- Validate atomization models
- Validate methodology for extending cold flow data to hot flow conditions
- Develop hot-flow correlations for direct use in combustion models

### **OBJECTIVE**

To characterize the flowfield downstream of a shear coaxial injector using LOX/GH<sub>2</sub> propellants under combusting conditions

- Drop size and velocity measurements using Phase Doppler Interferometry
- Laser sheet visualizations of near breakup region

### **FACILITY CAPABILITIES**

### **Propulsion Engineering Research Center Cryogenic Combustion Laboratory**

### **Propellants:**

Gaseous Hydrogen Gaseous Methane Gaseous Oxygen Liquid Oxygen

### Flow rates (maximum):

Gaseous oxygen: 0.1 lbm/s

Liquid oxygen: 1.0 lbm/s

Gaseous hydrogen: 0.25 lbm/s

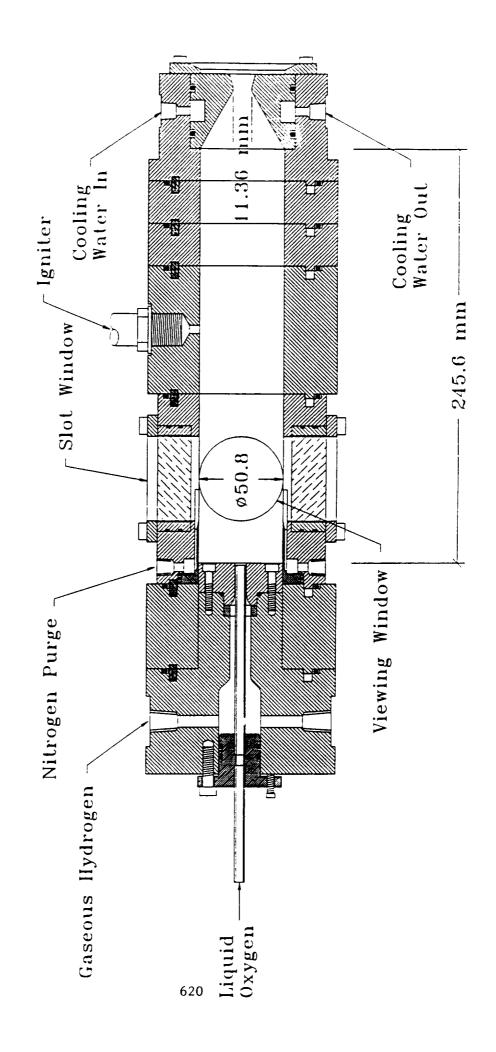
Typical mixture ratios: 4 - 8

Maximum chamber operating pressure: 1000 psi

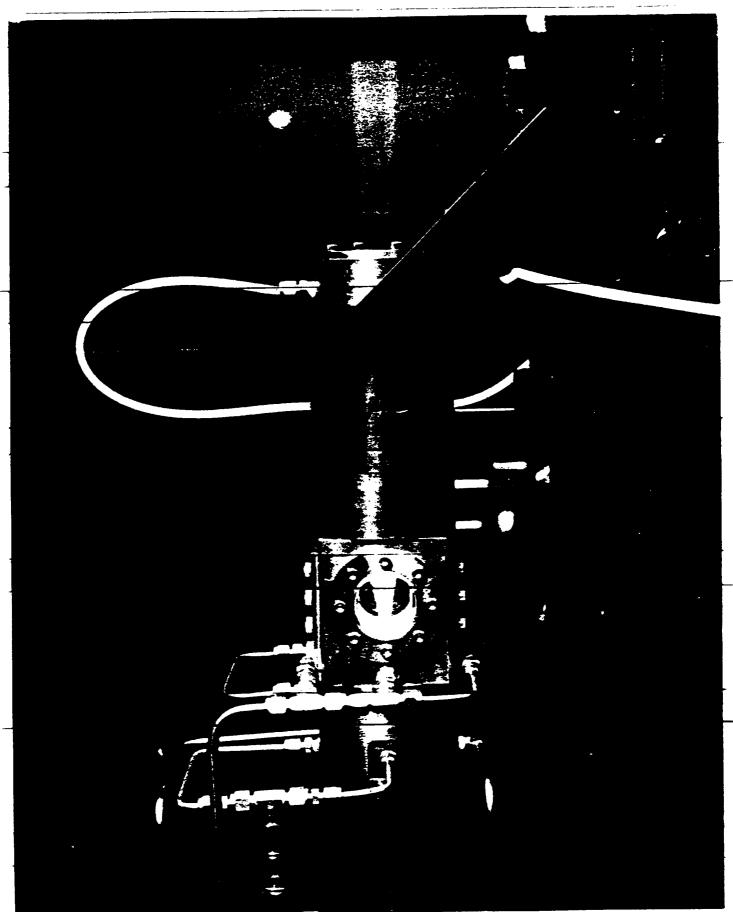
Typical test time: 1 - 5 s

Longer tests subject to hardware cooling and gas supply specifications

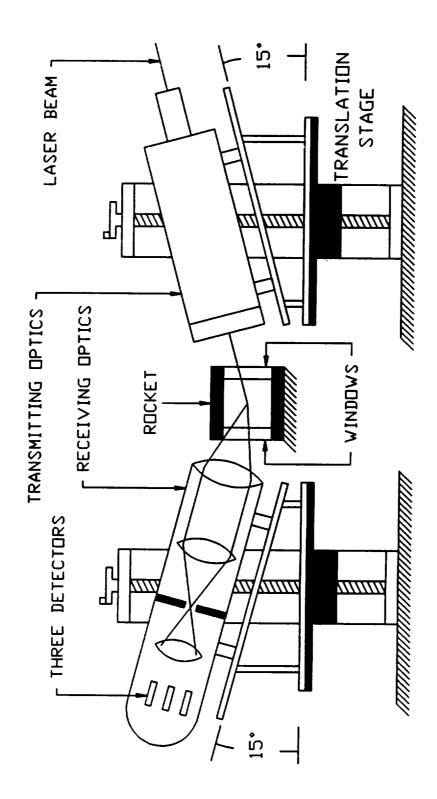
### PENN STATE ROCKET



Cross-Sectional View of the Windowed Rocket Chamber



## EXPERIMENTAL SCHEMATIC



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### **TEST CONDITIONS**

Chamber pressure 2.67 Mpa (387 psia)

LOX flowrate 0.112 kg/s (0.245 lbm/s)

 $GH_2$  flowrate 0.021 kg/s (0.045 lbm/s)

Mixture ratio (O/F) 5.4

LOX velocity 13.5 m/s (44.1 ft/s)

GH<sub>2</sub> velocity 381 m/s (1250 ft/s)

Momentum ratio (F/O) 5.22

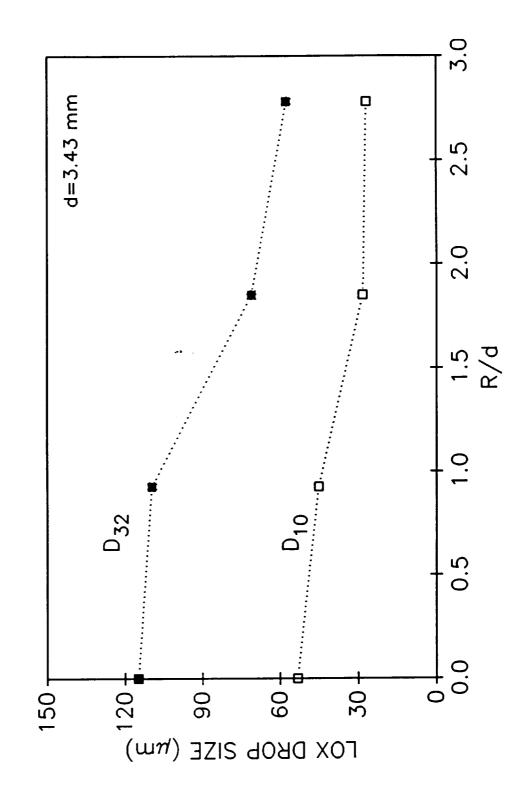
Velocity ratio (F/O) 28.3

Re<sup>1</sup> 5.03x10<sup>5</sup>

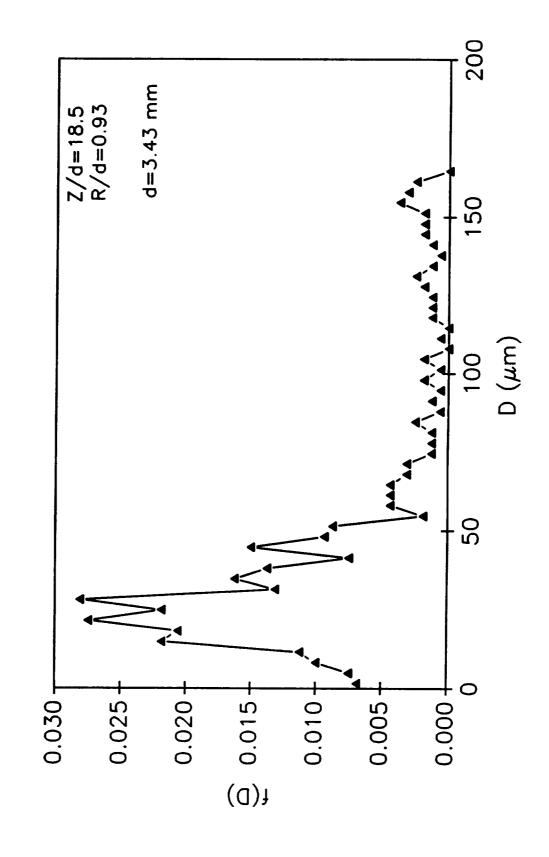
 $We^2$  2.06x10<sup>5</sup>

 ${}^{1}Re = \rho_{1}U_{1} d/\mu_{1}$   ${}^{2}We = \rho_{g}(U_{g}-U_{1})^{2}d/\sigma$ 

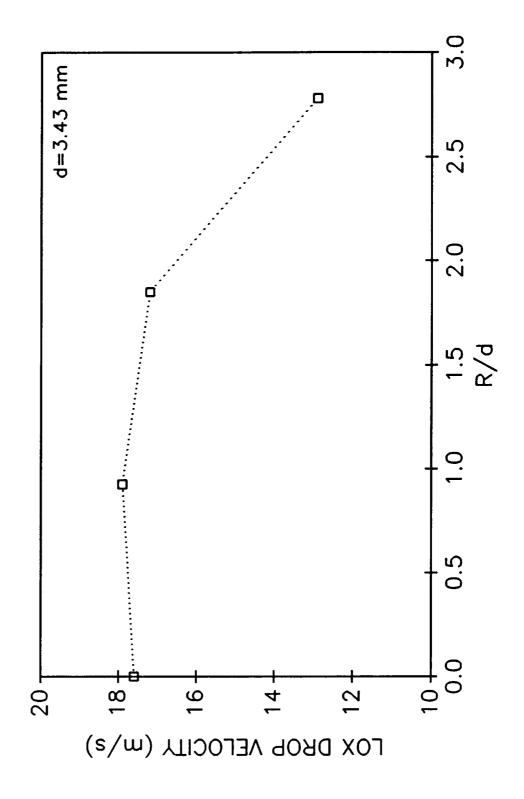
MEAN DROP DIAMETER VS. RADIAL LOCATION Z=63.5 mm (Z/d=18.5)



# LOX DROP SIZE DISTRIBUTION



MEAN DROP VELOCITY VS. RADIAL LOCATION Z=63.5 mm (Z/d=18.5)



### ROCKET PARAMETERS

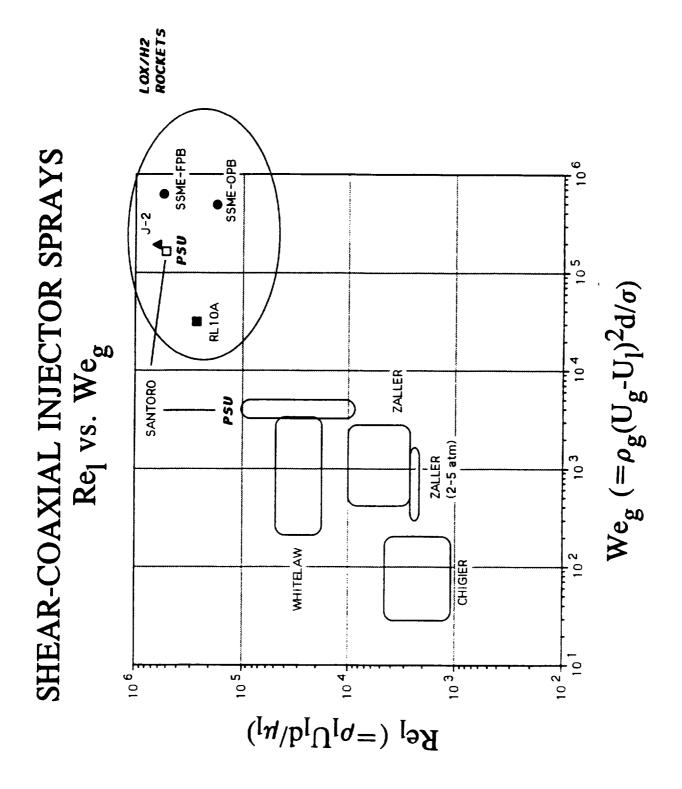
Run	Chamber Pressure (MPa)/	LOX Flowrate (kg/s)/	GH <sub>2</sub> Flowrate (kg/s)/	Mixture Ratio (O/F)	Momentum Ratio (F/O)	Velocity Ratio (F/O)	Re <sub>1</sub> 1 (x10 <sup>5</sup> )	$We_{(x10^5)}^2$
_	(psia) 2.79/404	0.120/ 0.264	0.021/ 0.047	5.6	4.70	26.8	4.97	1.61
2	2.72/395	0.110/	0.021/	5.2	5.58	29.2	5.11	1.95
ĸ	2.73/396	0.113/	0.021/	5.3	5.19	27.9	5.25	2.07
4	2.43/352	0.103/ 0.227	0.019/ 0.041	5.5	5.41	29.3	4.80	2.59

 ${}^{l}Re_{l} = \rho_{l}U_{l}d/\mu_{l}$  ${}^{2}We_{g} = \rho_{g}(U_{g}-U_{l})^{2}d/\sigma$ 

PDPA RESULTS

Axial Location, Z=63.5 mm (Z/d=18.5) LOX Post I.D., d=3.43 mm

Run	R/d	D <sub>10</sub> (μm)	$D_{10} (\mu m) D_{32} (\mu m) V (m/s)$	V (m/s)	# Drops % Val.	% Val.	Run Time (sec.)
	0.00	53.2	114.9	17.6	149	16%	1.41
2	0.93	45.1	109.7	17.9	484	21%	1.03
3	1.85	28.2	71.0	17.2	448	46%	1.52
4	2.78	26.8	57.5	12.9	45	62%	0.82



### **DROP SIZE EQUATIONS**

### NUKIYAMA/TANASAWA (1930) - E

$$\overline{D}_{12} = \frac{585}{V_r} \sqrt{\frac{\sigma}{\rho_l}} + 597 \left(\frac{\mu_l}{\sqrt{\sigma \rho_l}}\right)^{0.45} \left(1(XX) \frac{\dot{m}_l}{\rho_l} \frac{\rho_L}{\dot{m}_s}\right)^{1.5}$$

 $\overline{D}_{32} = 0.95 \left( \frac{\sigma^{0.33} m_0^{0.33}}{V_r \rho_l^{0.37} \rho_s^{0.33}} \right) \left( 1 + \frac{\dot{m}_l}{\dot{m}_s} \right)^{1.7} + 0.13 \mu_l \left( \frac{d}{\sigma \rho_l} \right)^{0.5} \left( 1 + \frac{\dot{m}_l}{\dot{m}_s} \right)^{1.7}$ 

\*LORENZETTO/LEFEBVRE (1977) - S/

### \*WEISS/WORSHAM (1959) - S/

$$\overline{D}_{\text{vol},s} = 0.61 \bigg( 1 + 1000 \frac{\rho_A}{\rho_l} \bigg) \bigg( \frac{V_r \mu_l}{\sigma} \bigg)^{\frac{1}{4}} \bigg( \frac{\sigma}{\rho_a V_r^2} \bigg) \bigg( \frac{\rho_l \sigma \mu_A}{\mu_l^4} \bigg( \dot{m}_l + \dot{m}_A \bigg) \bigg)^{\frac{1}{4}}$$

 $\overline{D}_{30} = 3.62 \left( \frac{\mu_s^{1.5}}{\rho_s \sigma^{1.5}} \right) \left( \frac{\dot{m}_t}{\dot{m}_s} \right)^{0.4} \frac{1}{V_c^{0.5}}$ 

\*ZALLER (1993) - S/

\*MAYER (1961) - 
$$SI$$

$$\overline{D}_{i,0,s} = 9\pi\sqrt{16}B\left(\frac{\mu_1\sqrt{\sigma}}{\rho_sV_s^2\sqrt{\rho_i}}\right)^{\frac{1}{2}}$$

Dimensionally Correct

English Units Metric Units

E S

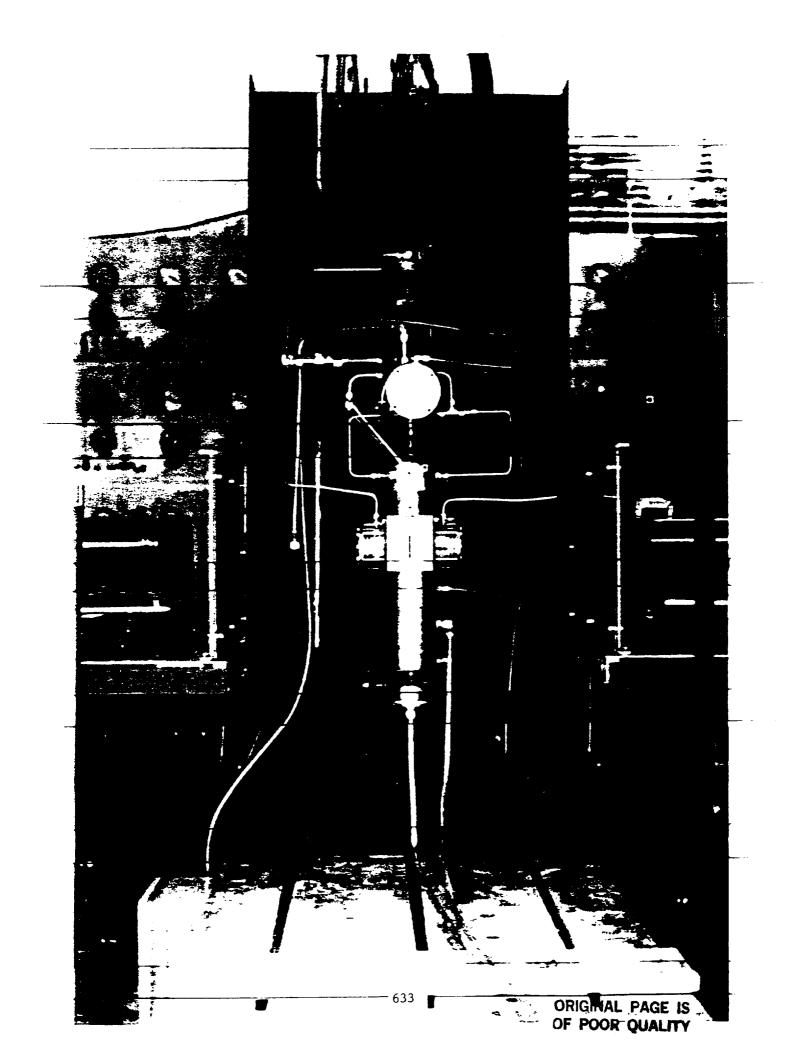
## DROP SIZE PREDICTIONS

CORRELATION	DROP DIAMETER	DROP SIZE $(\mu m)$ HOT FIRE <sup>1</sup>	DROP SIZE (μm) COLD FLOW <sup>2</sup>
NUKIYAMA (1939)	$D_{32}$	1227	2325
LORENZETTO (1977)	$D_{32}$	440	5856
WEISS (1959)	D <sub>v0.5</sub>	1.88	12.9
MAYER (1961)	D <sub>v0.5</sub>	0.39	4.25
ZALLER (1993)	$D_{30}$	4.8	64.9

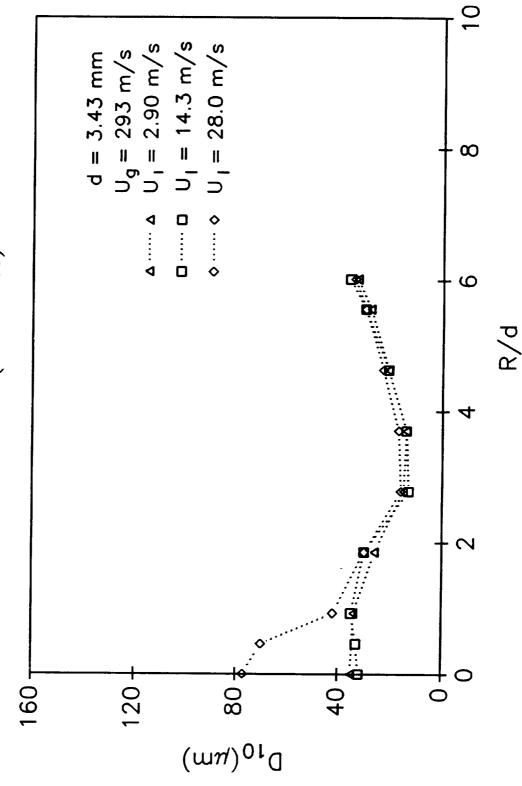
MEASURED DROP SIZE

 $^{1}$  HOT FIRE: 58 < D<sub>32</sub> < 115

 $^{2}$  COLD FLOW: 29 < D<sub>32</sub> < 88

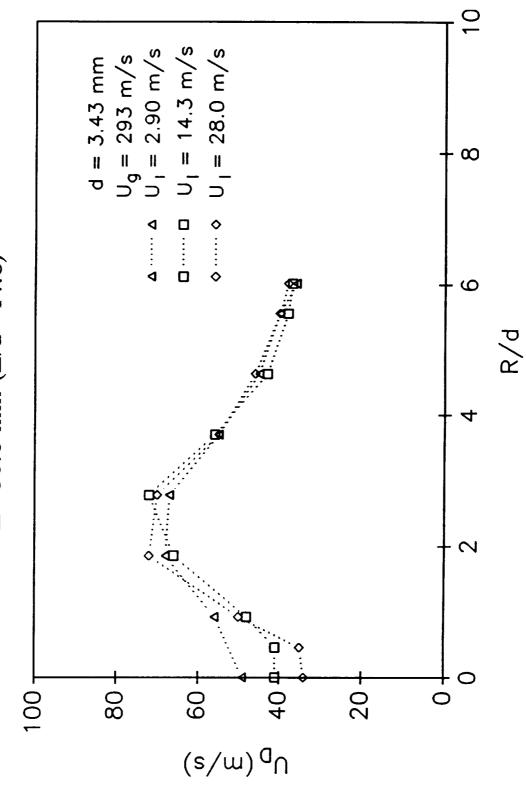


D<sub>10</sub> VS. RADIAL LOCATION H<sub>2</sub>O/GN<sub>2</sub> Atmospheric Tests Z=50.8 mm (Z/d=14.8)

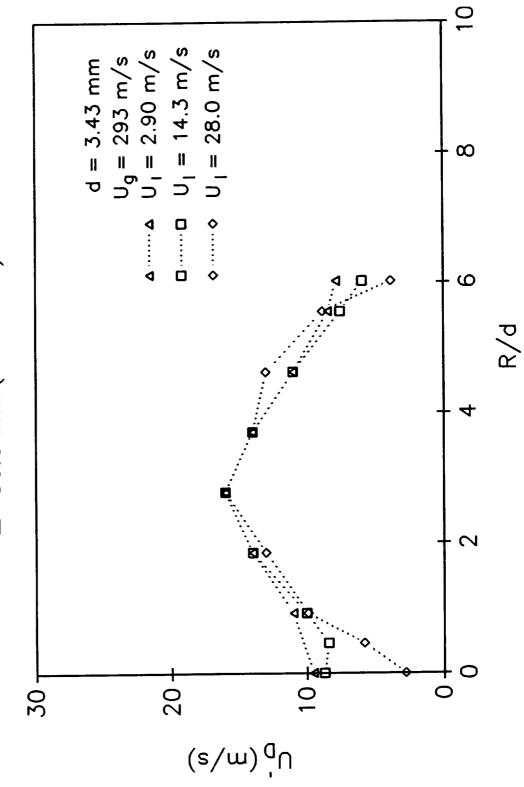


d = 3.43 mm  $U_g = 293 \text{ m/s}$   $U_1 = 2.90 \text{ m/s}$   $U_1 = 14.3 \text{ m/s}$   $U_1 = 28.0 \text{ m/s}$  $\infty$ D<sub>32</sub> VS. RADIAL LOCATION H<sub>2</sub>O/GN<sub>2</sub> Atmospheric Tests Z=50.8 mm (Z/d=14.8) .... Δ ..... Δ 9 2 120-80 0 160  $(m\eta)_{\Delta \Sigma}$ 

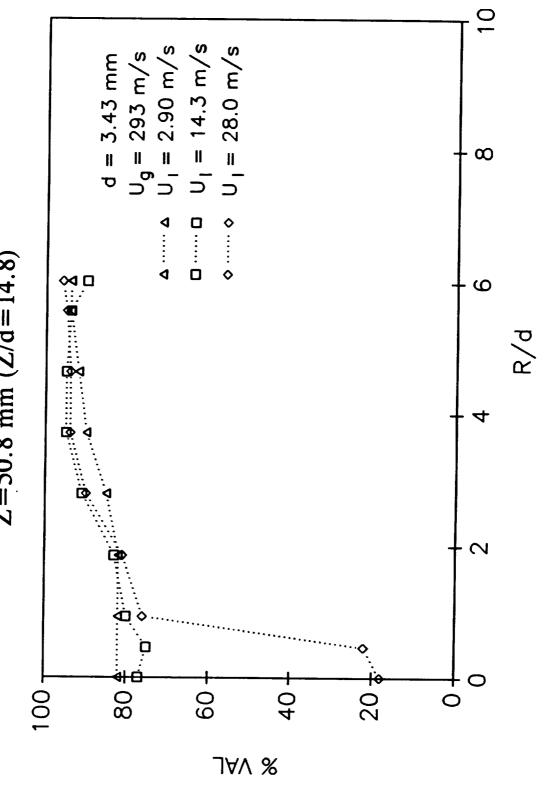
U<sub>D</sub> VS. RADIAL LOCATION H<sub>2</sub>O/GN<sub>2</sub> Atmospheric Tests Z=50.8 mm (Z/d=14.8)

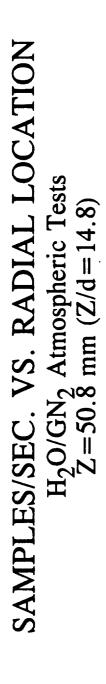


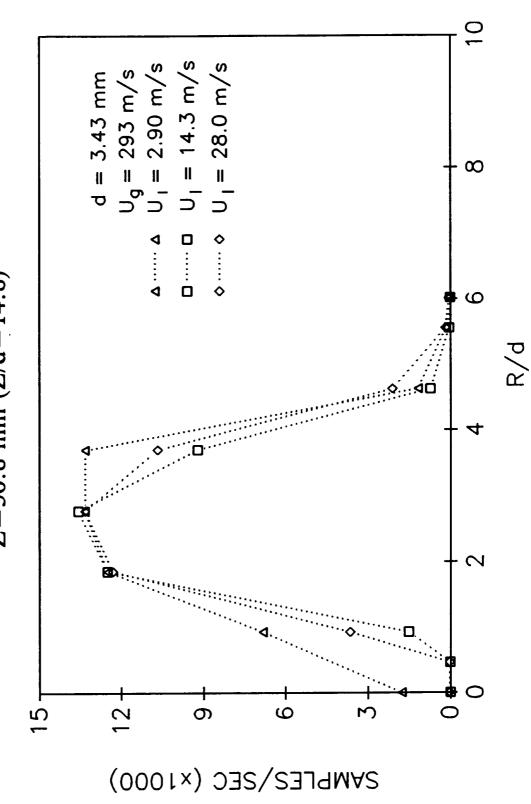
U<sub>D</sub>' VS. RADIAL LOCATION H<sub>2</sub>O/GN<sub>2</sub> Atmospheric Tests Z=50.8 mm (Z/d=14.8)



# % VALIDATION VS. RADIAL LOCATION H<sub>2</sub>O/GN<sub>2</sub> Atmospheric Tests Z=50.8 mm (Z/d=14.8)



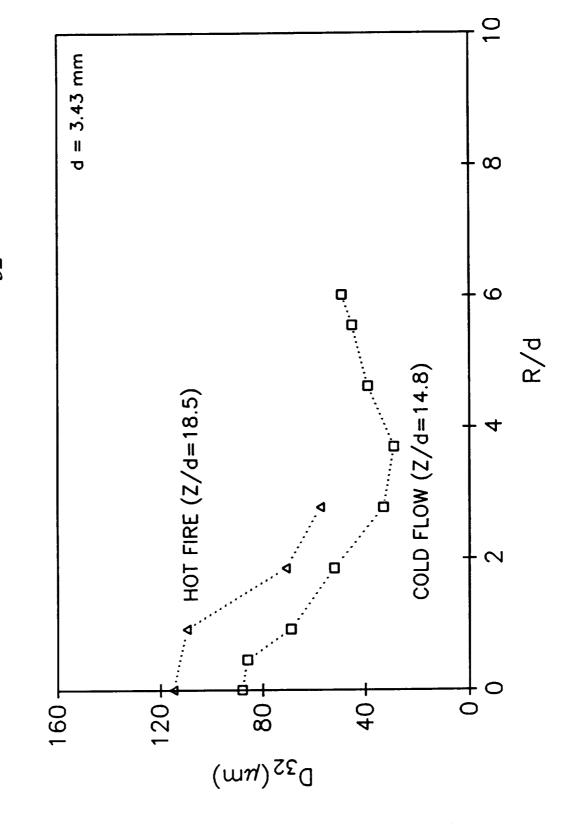




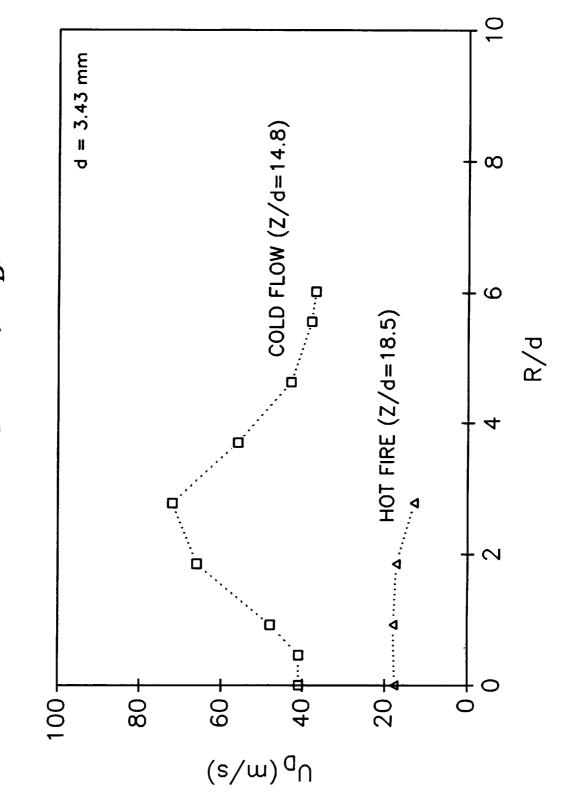
# HOT FIRE/COLD FLOW COMPARISON

	HOT FIRE	COLD FLOW	RATIO (H.F./C.F.)
CHAMBER PRESSURE (psia)	387	14.7	26.3
LIQUID FLOWRATE (kg/s)	0.112	0.13	0.85
GAS FLOWRATE (kg/s)	0.021	0.009	2.3
MIXTURE RATIO (O/F)	5.4	14.5	0.37
LIQUID VELOCITY (m/s)	13.5	14.3	0.94
GAS VELOCITY (m/s)	381	290	1.3
VELOCITY RATIO (F/O)	28.3	20.3	1.4
$Re_{l} (= \rho_{l} U_{l} d/\mu_{l})$	5.03 x 10 <sup>5</sup>	4.86 x 10 <sup>4</sup>	10.3
$We_g (= \rho_g (U_g - U_l)^2 d/\sigma)$	2.06 x 10 <sup>5</sup>	4.3 x 10 <sup>3</sup>	48

HOT FIRE/COLD FLOW COMPARISON Sauter Mean Diameter (D<sub>32</sub>)



HOT FIRE/COLD FLOW COMPARISON Mean Drop Velocity (UD)



### **SUMMARY**

- Measured liquid oxygen drop size and velocity in combusting environment
  - Intact core extends well beyond the injector
  - Drops confined to narrow region
- Correlations based on cold flow data inadequate for predicting drop size in LOX/GH<sub>2</sub> combusting flow
- Compared drop measurements between cold flow and combusting conditions for similar liquid and gas flowrates
  - Re<sub>1</sub> and We<sub>g</sub> differ by an order of magnitude
  - Mean drop size larger for hot fire conditions

### **ACKNOWLEDGEMENT**

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